

Chapter 2

Short Answer Problems

- The LMTD factor is required for heat exchangers when the two streams do not exhibit pure counter-current flow. Most exchangers such as S&T and other arrangements fall into this category.
- This statement is not generally true. In fact, condensers often have high heat transfer coefficients on the condensing side. One exception is for partial condensers where the majority of the condenser-side of the exchanger comprises of non-condensing gas – in this case the heat transfer coefficient on the condensing side may be limiting.
- Turbulent flow on both sides of the heat exchanger – see Table 2.9

a.	Shell-side	$h \propto Re_{0.6}$	$\frac{h}{h_{\text{base case}}} = \frac{1.5^{0.6}}{1}$	1.275 or and increase of 27.5%
b.	Tube-side	$h \propto Re_{0.8}$	$\frac{h}{h_{\text{base case}}} = \frac{1.5^{0.8}}{1}$	1.383 or and increase of 38.3%
- Laminar flow on both sides of the heat exchanger – see Table 2.9

a.	Shell-side	$h \propto Re_{0.45}$	$\frac{h}{h_{\text{base case}}} = \frac{1.5^{0.45}}{1}$	1.20 or and increase of 20%
b.	Tube-side	$h \propto Re_{0.3}$	$\frac{h}{h_{\text{base case}}} = \frac{1.5^{0.3}}{1}$	1.145 or and increase of 14.5%
- All else considered, the heat transfer coefficient for turbulent flow will be (much) higher than for laminar flow. For this reason when possible flow should be in the turbulent regime.
- Refer to Section 2.2.1.7 – three reasons for placing a fluid on the tube side of a S&T exchanger
 - 2-If the fluid is corrosive
 - 2-If the fluid causes severe fouling or scaling
 - 2-If the fluid is at a much higher pressure than the other fluid
 - 2-If the fluid has a much higher film coefficient
 - 2-If the material in contact with the fluid must be an expensive alloy

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Table of Contents **Solution Manual Chemical Process**

1. Understanding the eBook **Solution Manual Chemical Process**
 - The Rise of Digital Reading **Solution Manual Chemical Process**
 - Advantages of eBooks Over Traditional Books
2. Identifying **Solution Manual Chemical Process**
 - Exploring Different Genres
 - Considering Fiction vs. Non-Fiction
 - Determining Your Reading Goals
3. Choosing the Right eBook Platform
 - Popular eBook Platforms
 - Features to Look for in an **Solution Manual Chemical Process**
 - User-Friendly Interface
4. Exploring eBook Recommendations from **Solution Manual Chemical Process**
 - Personalized Recommendations
 - **Solution Manual Chemical Process** User Reviews and Ratings
 - **Solution Manual Chemical Process** and Bestseller Lists

5. Accessing Solution Manual Chemical Process Free and Paid eBooks
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 - ePub, PDF, MOBI, and More
 - Solution Manual Chemical Process Compatibility with Devices
 - Solution Manual Chemical Process Enhanced eBook Features
7. Enhancing Your Reading Experience
 - Adjustable Fonts and Text Sizes of Solution Manual Chemical Process
 - Highlighting and Note-Taking Solution Manual Chemical Process
 - Interactive Elements Solution Manual Chemical Process
8. Staying Engaged with Solution Manual Chemical Process
 - Joining Online Reading Communities
 - Participating in Virtual Book Clubs
 - Following Authors and Publishers Solution Manual Chemical Process
9. Balancing eBooks and Physical Books Solution Manual Chemical Process
 - Benefits of a Digital Library
 - Creating a Diverse Reading Collection Solution Manual Chemical Process
10. Overcoming Reading Challenges
 - Dealing with Digital Eye Strain
 - Minimizing Distractions
 - Managing Screen Time
11. Cultivating a Reading Routine Solution Manual Chemical Process
 - Setting Reading Goals Solution Manual Chemical Process
 - Carving Out Dedicated Reading Time
12. Sourcing Reliable Information of Solution Manual Chemical Process
 - Fact-Checking eBook Content of Solution Manual Chemical Process
 - Distinguishing Credible Sources
13. Promoting Lifelong Learning

- Utilizing eBooks for Skill Development
 - Exploring Educational eBooks
14. Embracing eBook Trends
- Integration of Multimedia Elements
 - Interactive and Gamified eBooks

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